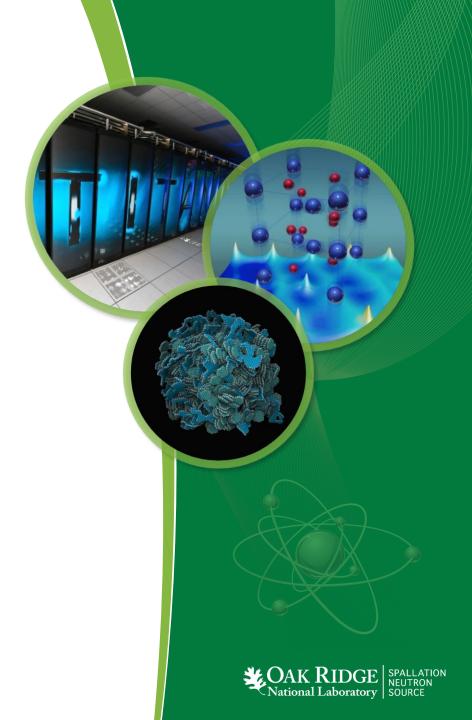
SNS Helium Cryogenic Plant Instrument and Controls Experience and Future Considerations

Presented at the Cryogenics Workshop 2016

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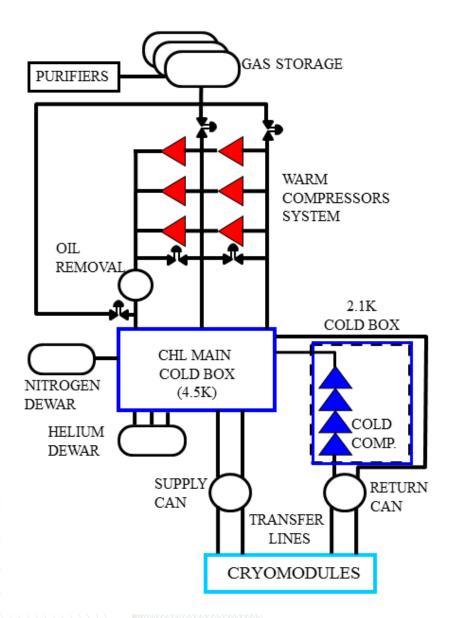
Outline

- SNS cryogenic system overview
- Cryogenic control system implementation
- Control sequence descriptions
- Control system Instrumentation
- Vendor Interface
- Failure Modes and Effects Analysis (FMEA)
- Lessons Learned
- Redundancy considerations
- Recommendations
- Summary

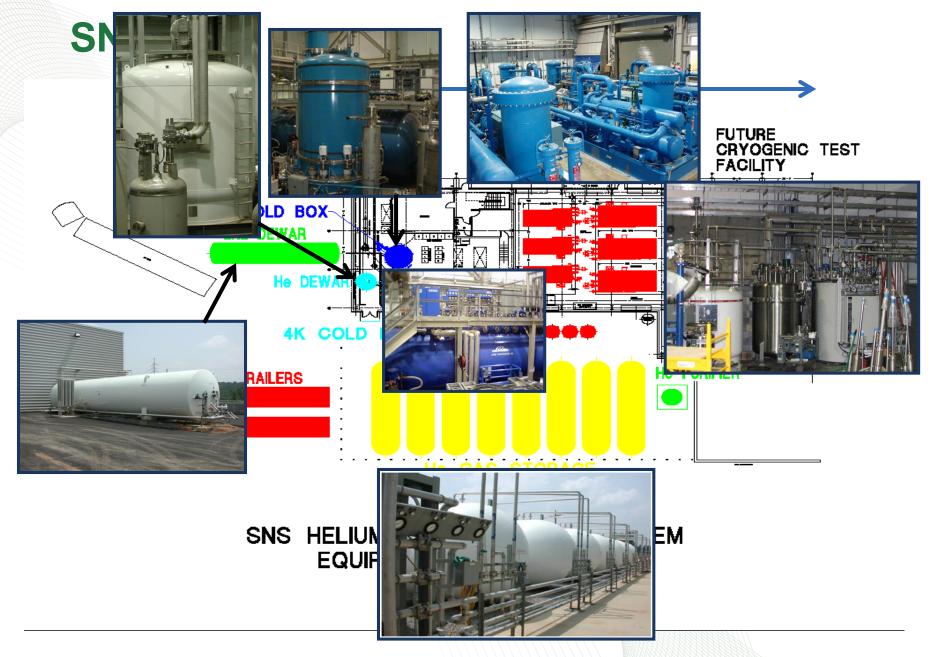


SNS CHL

- Design
 - 2400 watts at 2.1 K
 - 8300 watts shield cooling
 - 15 g/s liquefaction load for coupler cooling
 - Adequate margin for upgrades
- Provides cooling to the SCL
 - 11 medium beta cryomodules each housing three SCRF cavities
 - 12 high beta cryomodules each housing four SCRF cavities
 - 9 additional slots in linac for future upgrades











The SNS CHL Design Specifications

	Primary	Secondary	Shield
Supply Temperature	4.5K	4.5K	38K
Return Temperature	2.1K	300K	55K
Supply Pressure	3bar	3 bar	4 bar
Return Pressure	0.041bar	1.05 bar	3 bar
Static Load	850 W	5.0 g/s	6070 W
Dynamic Load	600 W	2.5 g/s	0
Capacity	125 g/s	15g/s	8300W

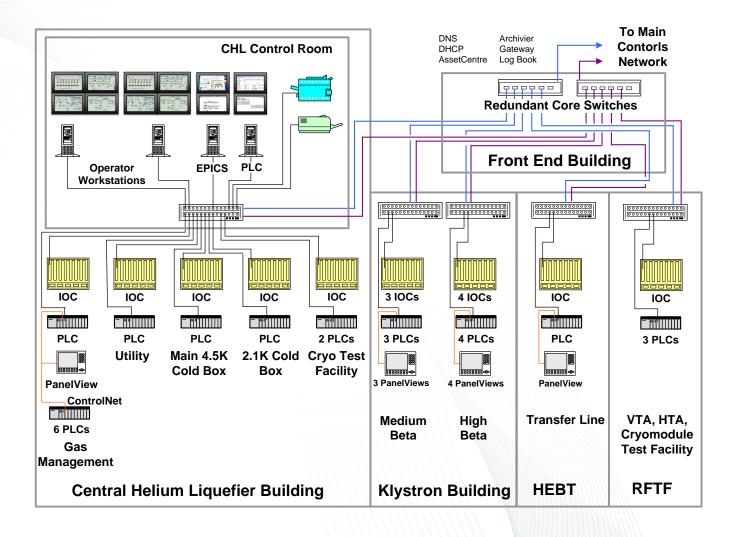


Control System Implementation

- EPICS based controls
- Requirements and features based on JLab cryo control system
- Dedicated network hardware and configuration
- EPICS VME IOCs (14)
 - Implement most subsystem upper level controls
 - Silicon Diode temperature sensor modules
 - LVDT position sensor modules
- Allen-Bradley ControlLogix PLCs (23)
 - Implement Interlocks and low level controls
 - Input/Output modules for monitoring sensors and controlling actuators
 - Profibus Communication modules for some devices



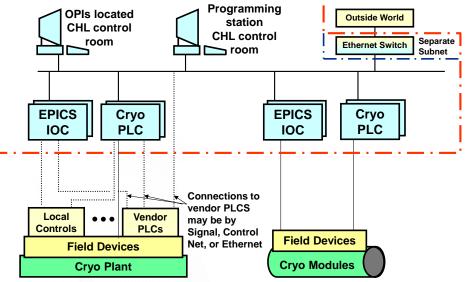
Cryogenic Control System Block Diagram





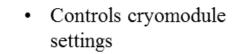
Control System Implementation

- Modular implementation using an IOC and PLC pair for each major subsystem
 - Main warm gas management, warm compressors
 - 4K Cold Box, 2K cold box, utility
 - Cryomodules
 - Minimizes overall system impact when working on one subsystem
- UPS power, backup power via Automatic Transfer Switches
- Soft IOCs (Linux based) Implement
 - Upper level sequences
 - Alarm notification

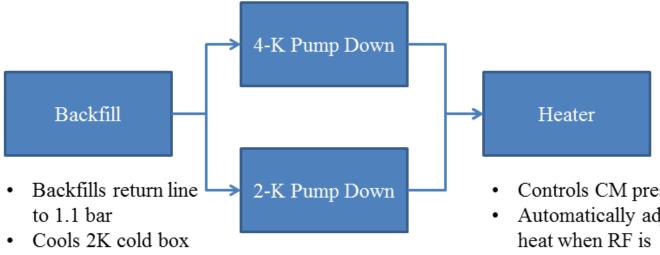




2K Control Sequences



Controls 4-K plant ٠



- Starts cold comp. at ٠ min. speed
- Establishes loop ٠ control of 2-K flow using CC4
- Sets gear ratios of ٠ CC1 - CC3

- Controls CM pressure
- Automatically adjusts applied to cavities



Control System Instrumentation

Pressure

- Moderate accuracy/resolution for most of plant
- High accuracy/resolution for 2K return at cold box inlet
- Radiation tolerant for cryomodule and Linac tunnel (strain gauge)
- Flow
 - Venturi (differential pressure) for most helium applications
 - Ultrasonic for some cooling water flows
 - Coriolis for high accuracy helium flow
- Temperature
 - Thermocouples or RTDs for "room temperature"
 - Silicon Diodes for cryo temperatures (standard curve)
 - Cernox for cryo temperatures (some individual curve, must track serial number, radiation resistant)
 - TVO; Russian developed carbon-aluminum oxide sensor (individual curve, must track serial number, radiation resistant)
 - CLTS; Cryogenic Linear Temperature Sensor

Control System Instrumentation

Level

- Differential pressure (mostly for LN)
- AMI liquid helium level probe and meter (2K and 4.5K versions)
- Speed
 - Magnetic sensor with signal conditioning
 - Frequency signal from VFDs
- Power
 - Dedicated power transducers for system capacity testing
 - MCC power transducers
 - Heater controller power signals



Vendor Interface

- Control system general requirements provided to vendors
 - Signal levels
 - Power available
 - Required documentation listing
 - Acceptable sensors and actuators
 - NRTL requirements
- Data received from vendors
 - Assembly and wiring drawings
 - Software descriptions
 - Operational descriptions
 - Interlock and control requirements
 - Test plans and procedures
 - Sample PLC logic
 - Sensor installation details (range, serial number, location, etc.)
 - Recommended spare parts list











Failure Modes and Effects Analysis of the CHL

- Breaks work down to task level for analysis
- Systematic approach asking two questions
 - How could this fail during this process task?
 - If it does fail, what is the effect based on severity, probability, and detection?
- This process delivers
 - Weaknesses in our process
 - Ranked items in need of focus
 - An opportunity for a group to focus on a process
 - A driving force to produce action
- Results of the FMEA
 - Probability X Severity X Detection = Risk Priority Number (RPN)
 - 60% decrease in RPN
 - Reduction of high risk items from 76 to less than 20
- Consider all modes of operation





Assigning Values and Calculate RPN

			Cl		Current Process				
Potential Failure Mode	Potential Effect(s) of Failure	Severity	Classification	Potential Cause(s) of Failure	Control Prevention	Occurance	Controls Detection	Detection	RPN
Trip a second stage compressor	Unable to maintain required flow to refrigerator, delayed trip of 4KCB	7		Oil Pump Trip	Preventative Maintenance	1	na**	7	49
		7			Monitor Temperature, Pressure, Oil Level, Visual Inspection	1	na**	7	49
		7		Skid PLC Failure	na**	10	na**	7	490
		7		High discharge pressure	System Controls	1	System alarm	1	7
		7		High discharge temperature	na**	1	na**	10	70
		7		High oil temperature	na**	1	na**	10	70
		7		Low oil inventory in skid separator	Procedural & Operator Training	1	Daily checksheet & Log	7	49



- Calibration Program initiated during commissioning
 - Stainless devices in stainless wells take a cheater bar
- Calibration records used numerous times during start-up and commissioning to verify proper system operation
- Difficult to calibrate instruments after system in operation
 - Usually requires system to be shut down
- Developing logic and screens to compare similar instruments to determine calibration needs
 - If all instruments on low pressure header read similar except one, go check the one



			_	T11004:P		_ Cal-			
Bar Code	No.		Signal	Name		Calibration Numb			
Required Accuracy			0.0	Unit	s atm	(sensor rang	0 - 34.023)		
			4	Unit	s atm				
		pressure se	nsor 4-20	Unit:	s ma	(v, ma)			
Authorized	Бу			Operation	s representa	ative authorizin	g removal from	n servic	
Measuren	nent and	Test Equipm				D	Calibratio		
1	Druck MC	Descri VII	iption		M210225	IU III	10/30/2002	on Date	
		oii Issure Module			3083	2	6/12/2002		
3	Druck Pre	ssure module			3003	5	6/12/2003		
4					-				
5									
Initial Re	eading	1.05 atm			noval from se	ervice	Time_ As Mea		
		7. Hange	psia	atm	tion values +/-	actual	PanelView	surea	
		0	psia N	a(m D	+/-	na	na		
		25	73.5						
							0.0		
				5.0	0.4	na	na		
		50	73.5 147.0 220.4	5.0 10.0 15.0	0.4	na na	na na		
		50	147.0	10.0	0.4	na	na		
Ac Calibr:	ated Data	50 75 100	147.0 220.4	10.0 15.0	0.4	na na	na na		
As Calibra	ated Data	50 75 100	147.0 220.4	10.0 15.0 20.0	0.4	na na	na na	sured	
As Calibra	ated Data	50 75 100	147.0 220.4	10.0 15.0 20.0	0.4 0.4 0.4	na na	na na na		
As Calibra	ated Data	50 75 100 % Range	147.0 220.4 293.9 psia 0	10.0 15.0 20.0 Calibra atm 0	0.4 0.4 0.4 tion Values +1- 0.4	na na na actual	na na na As Mea	EPIC	
As Calibra	ated Data	50 75 100 % Range 0 20	147.0 220.4 293.9 psia 0 58.8	10.0 15.0 20.0 Calibra atm 0 4.0	0.4 0.4 0.4 tion Values + <i>l</i> - 0.4 0.4	na na na actual 0.00 4.00	na na Na As Mea PanelView	EPIC	
As Calibra	ated Data	50 75 100 * Range 0 20 50	147.0 220.4 293.9 psia 0 58.8 147.0	10.0 15.0 20.0 Calibra atm 0 4.0 10.0	0.4 0.4 0.4 tion Values + / - 0.4 0.4 0.4	na na na actual 0.00 4.00 10.01	na na na As Mea PanelView	EPIC	
As Calibra	ated Data	50 75 100 * Range 0 20 50 80	147.0 220.4 293.9 0 58.8 147.0 235.1	10.0 15.0 20.0 Calibra atm 0 4.0 10.0 16.0	0.4 0.4 0.4 0.4 tion Values + / - 0.4 0.4 0.4 0.4 0.4	actual 0.00 4.00 10.01	na na na PanelView	EPIC 1	
As Calibra	ated Data	50 75 100 * * Range 0 20 50 50 80 100	147.0 220.4 293.9 psia 0 58.8 147.0 235.1 293.9	10.0 15.0 20.0 Calibra atm 0 4.0 10.0 16.0 20.0	0.4 0.4 0.4 tion Values +/- 0.4 0.4 0.4 0.4 0.4 0.4	na na na na actual 0.00 4.00 10.01 16.04 20.05	na na na As Mea PanelView	EPIC 1 1 2	
As Calibra	ated Data	50 75 100 * Range 0 20 50 80 100 80	147.0 220.4 293.9 9 0 58.8 147.0 235.1 293.9 235.1	10.0 15.0 20.0 Calibra atm 0 4.0 10.0 16.0 20.0 16.0	0.4 0.4 0.4 tion Values +1- 0.4 0.4 0.4 0.4 0.4 0.4 0.4	na na na na actual 0.00 4.00 10.01 16.04 20.05 16.06	na na na PanelView	EPIC (10 10 20 16	
As Calibra	ated Data	50 75 100 * Range 0 20 50 80 100 80 50	147.0 220.4 293.9 0 58.8 147.0 235.1 293.9 235.1 147.0	10.0 15.0 20.0 Calibra atm 0 4.0 10.0 10.0 10.0 16.0 20.0 16.0 10.0	0.4 0.4 0.4 0.4 +/- 0.4 0.4 0.4 0.4 0.4 0.4 0.4 0.4 0.4	na na na na actual 0.00 4.00 10.01 16.04 20.05 16.06 10.06	na na na PanelView	EPIC (10 16 20 16	
As Calibra	ated Data	50 75 100 8 7 7 8 0 20 50 80 100 80 50 50 20	147.0 220.4 233.9 0 58.8 147.0 235.1 235.1 235.1 235.9 235.1 235.1 235.9 235.1	10.0 15.0 20.0 Calibra atm 0 4.0 10.0 16.0 20.0 16.0 20.0 10.0 10.0 4.0	0.4 0.4 0.4 0.4 0.4 0.4 0.4 0.4	na na na na actual 0.00 4.00 10.01 16.04 20.05 16.06 10.06 4.09	na na na PanelView	EPIC (10 10 20 16 21 4	
		50 75 100 a 75 0 20 50 80 100 80 50 20 0	147.0 220.4 293.9 0 58.8 147.0 293.9 293.9 293.9 295.1 147.0 58.8 0	10.0 15.0 20.0 Calibra atm 0 4.0 10.0 16.0 20.0 16.0 10.0 4.0 0	0.4 0.4 0.4 tion Values +1- 0.4 0.4 0.4 0.4 0.4 0.4 0.4 0.4 0.4 0.4	na na na na actual 0.00 4.00 10.01 16.04 20.05 16.06 10.06	na na na PanelView	EPIC 11 11 21 11 21	
As Calibra Final Re		50 75 100 8 7 7 8 0 20 50 80 100 80 50 50 20	147.0 220.4 293.9 0 58.8 147.0 293.9 293.9 293.9 295.1 147.0 58.8 0	10.0 15.0 20.0 Calibra atm 0 4.0 10.0 16.0 20.0 16.0 10.0 4.0 0	0.4 0.4 0.4 0.4 0.4 0.4 0.4 0.4	na na na na actual 0.00 4.00 10.01 16.04 20.05 16.06 10.06 4.09	na na na PanelView	EPIC 11 11 21 11 21	
Final Re	ading	50 75 100 a 75 0 20 50 80 100 80 50 20 0	147.0 220.4 293.9 0 58.8 147.0 235.1 235.1 235.1 147.0 58.8 0	10.0 15.0 20.0 Calibra atm 0 4.0 10.0 16.0 20.0 16.0 10.0 4.0 0	0.4 0.4 0.4 tion Values +1- 0.4 0.4 0.4 0.4 0.4 0.4 0.4 0.4 0.4 0.4	na na na na actual 0.00 4.00 10.01 16.04 20.05 16.06 10.06 4.09	na na na PanelView	EPIC 11 11 21 11 21	
Final Re	ading n Label I	50 75 100 20 50 20 50 20 50 20 50 20 50 20 0 100 80 100 80 100 80 100 80 100 80 100 80 100 80 100 80 100 10	147.0 220.4 293.9 0 58.8 147.0 235.1 235.1 235.1 147.0 58.8 0	10.0 15.0 20.0 Calibra atm 0 4.0 10.0 20.0 16.0 20.0 16.0 10.0 4.0 0 After return	0.4 0.4 0.4 tion Values +1- 0.4 0.4 0.4 0.4 0.4 0.4 0.4 0.4 0.4 0.4	na na na na actual 0.00 4.00 10.01 16.04 20.05 16.06 10.06 4.09	na n	EPIC 11 11 21 11 21	

Expect 1	.1000 +/-	0.200) atm
	PT21102	1.0147	
1st Suct	PT21202	1.0286	
	PT21302	1.1318	OFF
Warm Gas	PT20103	1.0491	
	PT20501	1.0499	
4 K Cold Box	PT31610	0.8827	
	PT31106	1.0094	
	PT31119	1.0545	
	PT31136	1.0715	
	PT31159	1.1390	
	PT31190	1.0765	
	PT31198	1.0752	
2 K	PT41140H	1.2348	
Cold Box	PT41161	1.1612	

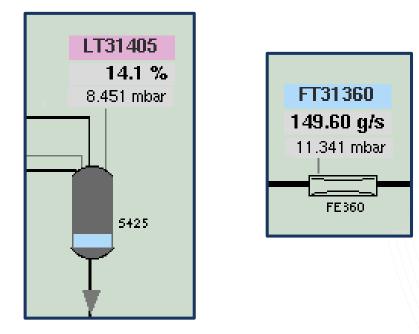
- Cryogenic control system must be implemented with cryo system operation requirements in mind
 - Modular, single subsystem per PLC/IOC
 - Highly reliable and available
 - Include test, calibration, and validation points and signals
 - Monitor operation of the control system itself
 - Communication errors, module status, signal status ...
 - Take appropriate action on detection of error
 - Easy to troubleshoot and quick to repair
- Global control system must support cryo control system operation
 - Servers must be available 100% of time
 - Network must be available 100% of time
 - Once cryo system starts, alarm handler and archiver for cryo cannot be stopped



- Communications
 - IOCs and PLCs must include logic to take appropriate action in the event of loss of communication
 - If the signal from sensor "X" is not valid, perform
 - Action A
 - Action B
 - If PLC "Y" cannot communicate with PLC "A", perform
 - Action C
 - Action D
 - Use FEMA process to determine appropriate actions
- Alarms, Auto-dialer or automatic personnel notification
 - For many cryogenic system disturbances, the appropriate automatic response is almost impossible to determine
 - Human intervention is required
 - Provide means for the control system to notify (with verification) appropriate personnel



- Displaying "Fail" state of valves (open closed)
- Displaying valve % on overview screens
 - Is the value an actual or a command?
- Displaying raw values for signals in addition to converted values
- Displaying control system hardware status

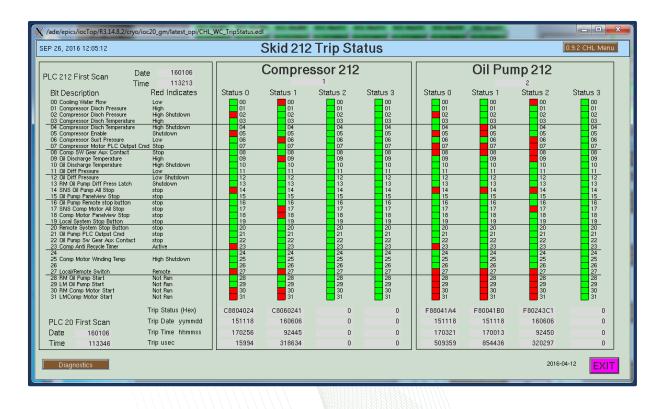


EC 0;	2, 2011	13:31:46		SCL	. PL	_C	Statu	S			
		PLC	54	I	ΗB	01	HB02	H	B03		
		Device Status	Ru	ın		ור	Major Fault	Re	c <mark>–</mark> –		1
		Key Switch	Re	emote		11	Minor Fault	Re	c –		1
		Force Status	N	o Force		11	Major Fault	Un	rec –		1
		Mode Change	N	ormal			Minor Fault	Un	rec 📒 -]
		Last Scan Time	15	598			Heartbeat		1590	00	
		Max Scan Time	55	519			Heartbeat A	lan	n ok		
	PLC R	lack Chassis 1	м	larshalli	ng Pa	nel	Chassis 3		FlexIO	Chassis 4	
Slot	Module	Status	Slot	Module	e	St	atus	[Slot Module	Status	
00	PLC	See Above	00	CNet		0			ACN15	0	
01	CNet	0	01	OB32		0			00 IRT8	15	00
02	ENet	0	02	-					01 IRT8	15	00
03	OB32	0	03	OB8		0			02 IRT8	15	00
04	IB32	0	04	OB8		0			03 IRT8	15	00
05	-		05	OB8		0		╎┝	04 IRT8	15	00
06	-		06	-				┥┝	05 IRT8	15	00
07	OF8	07 00	07	OB32		0		⊦⊢	06 -		
	IF16	1500	08					ΙL	07 -		
09	IF16	1500		-							
				-							
			11	-							
			12	-							
			13	-							
			14	- IF16	-	_	07				
			15	IF16			07			1	EVIT
				1010	_	_		J			EXIT

National Laboratory



- Include a status word(s) for every device that has automatic trip logic
 - Status work has a bit for every signal that can cause a trip
 - 0 = condition OK
 - 1 = condition bad
 - Include
 - Trip Time/Date
 - First Scan Time/Date





Redundancy considerations for control system

- Core and Aggregator switches
- Communication links from core/aggregator to edge switches
- Installed spare edge switches
 - Just move patch cables from failed switch to installed spare
- Power feeds for controls equipment
 - Equipment with dual power supplies preferred over Automatic Transfer Switches
- PLC processors for subsystems "hot" spare
 - Enables system update during operation
 - 4 K cold box
 - Cryomodule
 - Linac Distribution System
- PLC communication to Input/Output chassis
 - Continue running and repair communication problems on maintenance days
- Process instrumentation



Redundancy considerations for control system

- For 2K plants, primary return pressure
 - Low range pressure sensors at 2K box inlet (3 would be better to allow voting)
 - Ability to switch control functions between sensors during operation
- Cryomodule instrumentation
 - Helium level probes
 - Temperature sensors

Recommendations General

- For electrical safety considerations
 - Use NRTL equipment if available
 - Use 24 vdc signal and control devices
 - Use < 50 vdc heaters, actuators, if possible
- Use Ethernet communication to devices where possible
 - Avoid configuration issues
 - Do not use DeviceNet communication
 - Avoid ControlNet communication
 - Limits our ability to add new control system equipment
- Wiring terminals
 - Screw terminals are easy to over torque, under torque, intermittent connections
 - Spring clamp terminals have almost no intermittent connections
- Move more control to the PLC





Recommendations, Standardization

PLC system

- Pick a vendor and stay with them
- Even if the "standard PLC" is overkill for a function, having standard programming software and spare parts is valuable
- Pick "standard" I/O modules for each type signal (AI, AO, BI, BO)
- Instrumentation
 - Lots of good instrumentation vendors, try to stay with 2 or 3
- Include PLC and instrumentation requirements when procuring "turn-key" systems



Summary

- We have learned much about the cryogenic control system throughout the first ten years of operation
- The system has proven to be robust and reliable but there are opportunities for improvement
- Consider all modes of operation when developing the control system
- Answer the question of "how are we going to maintain this system?" during design
- Redundancy and standardization are key characteristics of a control system

